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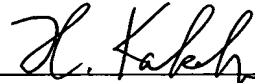
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DESCRIPTION

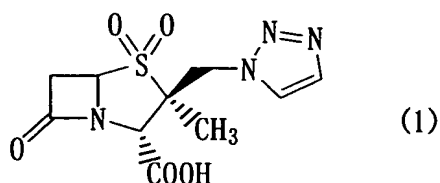
PENAM CRYSTALS AND PROCESS FOR PRODUCING THE SAME

TECHNICAL FIELD

5 The present invention relates to penam crystals and a process for producing the same.

BACKGROUND OF THE INVENTION

Formula (1):



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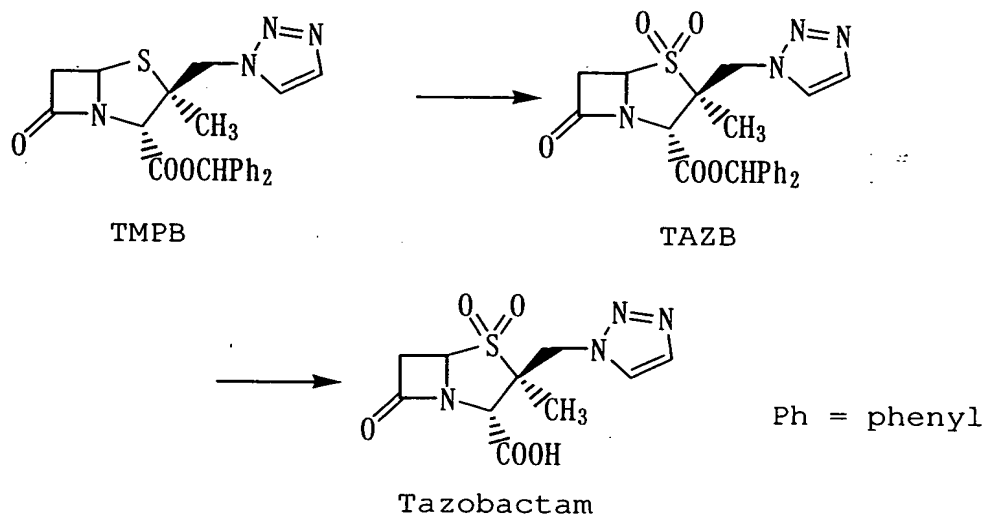
Tazobactam, which is represented by Formula (1) given above, exhibits very weak antibacterial activity, and it is therefore not used alone as an antibacterial agent. However, it irreversibly binds to various β -lactamases produced by microorganisms and exhibits an ability to inhibit β -lactamase activities. Hence, tazobactam is used in combination with various existing antibacterial agents that are inactivated by β -lactamases, allowing such antibacterial agents to exhibit their inherent antibacterial activity against β -lactamase-producing microorganisms (Katsuji SAKAI, *Recent Antibiotics Manual*, 10th ed., page 113).

15

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As shown in the reaction scheme below, tazobactam is produced by oxidizing 2 α -methyl-2 β -[(1,2,3-triazol-1-yl)methyl]penam-3 α -carboxylic acid benzhydryl ester (hereinafter sometimes referred to as "TMPB") and de-esterifying the resulting 2 α -methyl-2 β -[(1,2,3-triazol-1-yl)methyl]penam-3 α -carboxylic acid 1,1-dioxide benzhydryl ester (hereinafter sometimes referred to as "TAZB") thus obtained. Therefore, TMPB is of use as an intermediate for synthesizing tazobactam and as a precursor of TAZB.

Reaction Scheme:



Since the nucleophilic 1,2,3-triazol moiety is contained in the TMPB molecule, oily or amorphous TMPB is unstable and likely to undergo decomposition, degeneration, etc. For this reason, efforts have been made to isolate

crystalline TMPB, which is stable (WO02/14325).

The method disclosed in WO02/14325 produces TMPB crystals by concentrating a TMPB-containing solution, diluting the concentrated solution with an acetic acid ester, and mixing the diluted solution with hexane or like solvent.

However, in the method disclosed in WO02/14325, the efficiency of separating TMPB from by-products that are simultaneously generated in the reaction is low. Therefore, to obtain highly pure TMPB crystals, large amounts of TMPB inevitably remain in the mother liquor, resulting in a low yield of TMPB crystals.

DISCLOSURE OF THE INVENTION

An object of the present invention is to provide a process for producing highly pure TMPB in a high yield.

The inventors conducted extensive research to solve the problem described above and, as a result, succeeded in developing novel TMPB-acetone crystals that can be a precursor of TAZB. Furthermore, the inventors found that such TMPB-acetone crystals can be readily produced and efficiently isolated from a solution prepared by concentrating a TMPB-containing solution and dissolving the concentrated solution in acetone, and also found that TMPB crystals can be produced in high purity and high

yield by de-acetonizing such TMPB-acetone crystals. The present invention has been accomplished based on these findings.

The present invention is as described in the
5 following Items 1 to 22 below:

1. TMPB-acetone crystals.

2. Crystals according to Item 1 that have a peak
at an interplanar spacing of 11.24 to 12.44 Å in the X-ray
powder diffraction pattern obtained by copper radiation of
10 $\lambda=1.5418$ Å through a monochromator.

3. Crystals according to Item 1 that have peaks
at the following interplanar spacings in the X-ray powder
diffraction pattern obtained by a copper radiation of
 $\lambda=1.5418$ Å through a monochromator:

15 d (Interplanar spacings)

11.24-12.44

8.41-9.30

4. Crystals according to Item 1 that have peaks
at the following interplanar spacings in the X-ray powder
20 diffraction pattern obtained by a copper radiation of
 $\lambda=1.5418$ Å through a monochromator:

d (Interplanar spacings)

11.24-12.44

8.41-9.30

25 7.11-7.87

5.62-6.22

3.78-5.12

5. Crystals according to Item 1 that have peaks
at the following interplanar spacings in the X-ray powder
5 diffraction pattern obtained by a copper radiation of
 $\lambda=1.5418 \text{ \AA}$ through a monochromator:

d (Interplanar spacings)

11.248-12.433

8.413-9.298

10 7.119-7.868

5.621-6.213

4.632-5.119

4.548-5.026

4.457-4.926

15 4.206-4.648

4.132-4.567

3.738-4.131

3.785-4.183

6. Crystals according to any one of Items 1 to 5
20 that have a TMPB/acetone molar ratio of 1/1.

7. A process for producing TMPB-acetone crystals
comprising the steps of:

(A) concentrating a TMPB-containing organic
solvent solution;

25 (B) dissolving the resulting concentrate in

acetone; and

(C) precipitating TMPB-acetone crystals from the acetone solution thus obtained.

8. A process according to Item 7, wherein the
5 organic solvent in Step A is a halogenated hydrocarbon solvent.

9. A process according to Item 8, wherein the halogenated hydrocarbon solvent is dichloromethane.

10. A process according to any one of Items 7 to
10 9, wherein in Step (A) the amount of organic solvent is reduced to about 1.5 liters or less per kg of TMPB.

11. A process according to any one of Items 7 to
10, wherein in Step (B) acetone is used in an amount of from about 1.5 to about 5 liters per kg of TMPB contained
15 in the concentrate.

12. A process according to any one of Items 7 to 11, wherein the TMPB-acetone crystals are precipitated by cooling the acetone solution.

13. A process according to any one of Items 7 to
20 11, wherein the TMPB-acetone crystals are precipitated by adding to the acetone solution a poor solvent for TMPB-acetone crystals.

14. A process according to Item 13, wherein the poor solvent is at least one member selected from the
25 group consisting of C₄₋₈ aliphatic hydrocarbons, C₄₋₈

alicyclic hydrocarbons and C₂₋₁₀ alkyl ethers.

15. A process according to Item 14, wherein the poor solvent is at least one member selected from the group consisting of *n*-pentane, *n*-hexane, *n*-heptane, *n*-
5 octane, cyclohexane, diethyl ether, di-*n*-butyl ether, diisopropyl ether and diisobutyl ether.

16. A process according to Item 15, wherein the poor solvent is *n*-hexane.

17. A process for producing TAZB comprising the
10 step of reacting TMPB-acetone crystals in a solvent with an oxidizing agent.

18. A process according to Item 17, wherein the oxidizing agent is at least one member selected from the group consisting of permanganic acid, periodic acid,
15 peracetic acid, trifluoroperacetic acid, perbenzoic acid, *m*-chloroperbenzoic acid, alkali metal salts thereof, and hydrogen peroxide.

19. A process for producing TMPB crystals comprising the step of de-acetonizing TMPB-acetone
20 crystals.

20. A process according to Item 19, wherein the TMPB-acetone crystals subjected to de-acetonization under reduced pressure.

21. A process according to Item 20, wherein the
25 de-acetonization is carried out at a pressure of from

about 1 to about 10 kPa and at a temperature of about 20°C or higher.

22. A process for producing TMPB crystals comprising the steps of:

5 (A) concentrating a TMPB-containing organic solvent solution;

(B) dissolving the resulting concentrate in acetone;

(C) precipitating TMPB-acetone crystals from the
10 acetone solution thus obtained; and

(D) de-acetonizing the TMPB-acetone crystals.

TMPB-acetone crystals

The TMPB-acetone crystals of the present
15 invention can be produced using, for example, Steps (A) to (C) below:

Step A

This step is for concentrating a TMPB-containing organic solvent solution.

20 TMPB-containing organic solvent solutions usable in this step include TMPB-containing reaction solutions obtained according to known methods.

Organic solvents include those that are usable in reactions for producing TMPB, or in TMPB extraction.

25 Preferable are hydrophobic organic solvents. Examples of

such hydrophobic organic solvents are dichloromethane,
1,2-dichloroethane, 1,2-dichloropropane, 1,1,2-
trichloroethane, chloroform, carbon tetrachloride, and
like halogenated hydrocarbon solvents. Among such
5 solvents, dichloromethane is particularly preferable.

Concentration of TMPB-containing organic
solvents can be carried out according to known techniques.
Concentration is preferably carried out under reduced
pressure, for example, at a pressure of from about 25 to
10 about 80 kPa.

In the present invention, concentration of
organic solvent solutions refers to complete removal of
organic solvents and partial removal of organic solvents
by which organic solvent remains in the concentrate. It
15 is usually sufficient that the amount of organic solvent
is concentrated to be not more than about 1.5 liters per
kg. of TMPB. In view of precipitation efficiency, it is
preferably from about 0.15 to about 0.7 liters, and more
preferably from about 0.2 to about 0.5 liters, per kg of
20 TMPB.

Step B

This step is for dissolving in acetone the
concentrate obtained in Step A.

In this step, it is sufficient that acetone is
25 used in an amount of from 1.5 to 5 liters, preferably from

2 to 4 liters, and more preferably from 2.2 to 3 liters, per kg of TMPB contained in the concentrate. When an organic solvent is present in the concentrate, acetone is preferably used in an amount such that the volume ratio of organic solvent/acetone is not more than 1/3, and preferably not more than 1/4.

In dissolving the aforementioned concentrate in acetone, when the concentrate is heated to aid dissolution, the concentrate should not be heated to a temperature of higher than about 40°C in view of the stability of TMPB, and it is preferable to avoid heating TMPB for a long time.

Step C

This step is for precipitating TMPB-acetone crystals from the acetone solution obtained in Step B.

Precipitation can be carried out according to conventional precipitation methods. For example, precipitation can be carried out by cooling the acetone solution or adding to the acetone solution a poor solvent for TMPB-acetone crystals.

When crystals are precipitated by cooling the acetone solution, the acetone solution is usually cooled to about 10°C or lower and preferably about 0°C or lower.

Solvents that have compatibility with acetone and poor ability to dissolve TMPB are widely used as poor solvents for TMPB-acetone crystals.

Examples of such poor solvents are C₄₋₈ aliphatic hydrocarbons, C₄₋₈ alicyclic hydrocarbons, C₂₋₁₀ alkyl ethers, etc. Such poor solvents can be used singly or in combination.

5 Specific examples of C₄₋₈ aliphatic hydrocarbons and C₄₋₈ alicyclic hydrocarbons are *n*-pentane, *n*-hexane, *n*-heptane, *n*-octane, cyclohexane, etc.

 Specific examples of C₂₋₁₀ alkyl ethers are diethyl ether, diisopropyl ether, di-*n*-butyl ether,
10 diisobutyl ether, etc.

 Among such poor solvents, C₄₋₈ aliphatic hydrocarbons are preferable, with *n*-hexane being particularly preferable.

 Although the amount of poor solvent is not
15 limited, in view of precipitation efficiency and workability, it is usually from about 0.1 to about 20 liters, and preferably from about 0.5 to about 5 liters, per liter of acetone contained in the acetone solution.

 The precipitation temperature is usually about
20 56°C or lower, preferably from about -78 to about 30°C and more preferably from about -30 to about 10°C.

 TMPB-acetone crystals precipitated as above can be separated from the acetone solution according to known filtration methods.

25 TMPB-acetone crystals thus obtained have a

TMPB/acetone molar ratio of 1/1 and exhibit a specific X-ray powder diffraction pattern.

The TMPB-acetone crystals of the invention have a peak at an interplanar spacing of 11.24 to 12.44 Å in
5 the X-ray powder diffraction pattern obtained by copper radiation of $\lambda=1.5418$ Å through a monochromator.

The preferable TMPB-acetone crystals of the invention have peaks at the following interplanar spacings in the X-ray powder diffraction pattern obtained by a
10 copper radiation of $\lambda=1.5418$ Å through a monochromator:
d (Interplanar spacings)

11.24-12.44

8.41-9.30

More preferable TMPB-acetone crystals of the
15 invention have peaks at the following interplanar spacings in the X-ray powder diffraction pattern obtained by a copper radiation of $\lambda=1.5418$ Å through a monochromator:
d (Interplanar spacings)

11.24-12.44

20 8.41-9.30

7.11-7.87

5.62-6.22

3.78-5.12

Particularly preferable TMPB-acetone crystals of
25 the invention have peaks at the following interplanar

spacings in the X-ray powder diffraction pattern obtained by a copper radiation of $\lambda=1.5418 \text{ \AA}$ through a monochromator:

d (Interplanar spacings)

5	11.248-12.433
	8.413-9.298
	7.119-7.868
	5.621-6.213
	4.632-5.119
10	4.548-5.026
	4.457-4.926
	4.206-4.648
	4.132-4.567
	3.738-4.131
15	3.785-4.183

An X-ray diffraction spectral analysis shows that the TMPB-acetone crystals of the invention have a crystalline structure completely different from that of known TMPB crystals. A ^1H -NMR spectral analysis shows the presence of TMPB at a TMPB/acetone molar ratio of 1/1. A thermogravimetric analysis also reveals the presence of TMPB and acetone at a molar ratio of 1 : 1 and the occurrence of acetone elimination at a temperature (83.2°C) higher than the boiling point of acetone. Therefore, it is presumed that acetone is not adhered to

TMPB due to insufficient drying, but that acetone is present throughout the crystal lattice of TMPB, thereby forming a clathrate.

TAZB production

5 TAZB is produced by reacting the TMPB-acetone crystals of the invention with an oxidizing agent in a solvent.

 Known oxidizing agents can be widely used, and examples thereof are permanganic acid, periodic acid,
10 peracetic acid, trifluoroperacetic acid, perbenzoic acid, *m*-chloroperbenzoic acid, alkali metal salts thereof, and hydrogen peroxide. Alkali metals as used herein include sodium, potassium, etc. Such oxidizing agents can be used singly or in combination.

15 Although such oxidizing agent may be used in a large excess relative to the TMPB-acetone crystals, it is usually sufficient to use the oxidizing agent in an amount of 1 to 5 moles per mole of the TMPB-acetone crystals.

 Examples of the solvent are dichloromethane,
20 chloroform, carbon tetrachloride and like halogenated hydrocarbons; tetrahydrofuran, dioxane and like ethers; acetone, methyl ethyl ketone and like ketones; acetic acid, formic acid and like organic acids; pyridine; water, etc. Such solvents can be used singly or in combination.

25 Such solvents are usually used in an amount of

from about 0.001 to about 100 liters, and preferably from about 0.01 to about 10 liters, per kg of TMPB-acetone crystals, but the amount of the solvent is not limited to the above range.

5 Although the temperature for reaction with oxidizing agents is not limited, about 0 to about 60°C is usually sufficient. The reaction time is usually from about 0.5 to about 12 hours.

TAZB thus produced can be purified according to
10 conventional purification methods such as extraction, column chromatography, recrystallization, etc.

TMPB crystal production

The TMPB-acetone crystals of the invention very slowly change to TMPB crystals at atmospheric pressure and
15 room temperature (20°C). To produce highly pure TMPB crystals such that TMPB-acetone crystals cannot be detected, it is preferable to carry out de-acetonization.

De-acetonization may be carried out by, for example, maintaining the TMPB-acetone crystals under
20 reduced pressure. Although the extent of pressure reduction is not limited, a pressure of, for example, from about 1 to about 10 kPa, and preferably from about 1.3 to about 5 kPa, is sufficient. It is further preferable to maintain the ambient temperature of the TMPB-acetone
25 crystals usually at about 20°C or higher, preferably 30°C

or higher and more preferably from about 30 to about 40°C. Excessively high ambient temperatures possibly result in degradation of the TMPB crystals.

5 The de-acetonization time cannot be generalized since it varies depending on the extent of pressure reduction, temperature, etc. For example, de-acetonization takes 6 hours or longer at about 4 kPa and about 40°C.

10

EFFECTS OF THE INVENTION

One of the advantages of the process for producing TMPB-acetone crystals of the present invention is its great crystallization efficiency. It is presumed that TMPB in acetone forms a clathrate in conjunction with
15 acetone, which is distinct from TMPB alone, and thereby the compatibility with acetone is decreased and TMPB-acetone crystals are more readily precipitated.

Therefore, in the production of the TMPB-acetone crystals of the invention, the precipitation temperature
20 is not limited, allowing sufficient precipitation to occur at room temperature. Moreover, cooling does not permit contamination by other components or separation of oily material.

The TMPB-acetone crystals of the invention can
25 be used as they are in the production of TAZB.

Moreover, TMPB crystals can be readily produced by de-acetonizing the TMPB-acetone crystals of the invention. In particular, TMPB crystals can be produced in high yield and high purity by forming crystals composed of TMPB and acetone, which can be recovered extremely efficiently, and then de-acetonizing the TMPB-acetone crystals.

According to the process for producing TMPB crystals of the invention, TMPB crystals are produced by way of producing TMPB-acetone crystals, which can be efficiently precipitated, thereby not allowing contamination with by-product cepham compounds and readily enabling TMPB crystals to be obtained from TMPB-acetone crystals.

Therefore, the method of the invention is highly industrially advantageous.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is the x-ray powder diffraction pattern of the crystals obtained in Example 1.

Figure 2 is the x-ray powder diffraction pattern of the crystals obtained in Example 8.

BEST MODE FOR CARRYING OUT THE INVENTION

Examples and a Comparative Example are given

below to describe the invention in more detail. However, the scope of the invention is not limited to or by these examples.

Example 1

5 A dichloromethane solution (700ml) containing
43.5 g of 2 β -chloromethyl-2 α -methylpenam-3-carboxylic acid
benzhydryl ester was mixed with 200 ml of 1,2,3-triazole
and about 130 ml of an anion exchange resin ("Diaion WA30",
manufactured by Mitsubishi Chemical Corp.), and the mixture
10 was stirred at 40°C for 3 hours. After the reaction, the
anion exchange resin was filtered off, and 200 ml of water
was added to the filtrate to separate the dichloromethane
layer. The dichloromethane layer thus obtained was washed
twice with water, thereby giving 600 ml of a
15 dichloromethane solution. This dichloromethane solution is
hereinafter referred to as "dichloromethane solution (1)".
This solution contained 30 g of TMPB.

Dichloromethane solution (1) was concentrated
under reduced pressure (60 to 40 kPa) at 40°C or lower.
20 When about 450 ml of dichloromethane was removed, 250 ml of
acetone was added to the thus-concentrated dichloromethane
solution (1). Concentration was continued until the amount
of the solution reached about 100 ml. A gas
chromatographic analysis revealed about 30 ml of acetone
25 and about 15 ml of dichloromethane. To this solution was

added acetone in such an amount that the total amount of acetone in the resulting solution was 80 ml. This solution is hereinafter referred to as "acetone solution (1)".

Acetone solution (1) was cooled to -20°C and stirred. After sufficient crystal precipitation, the crystals precipitated were recovered by filtration and washed with 80 ml of acetone/*n*-hexane mixture (volume ratio=1:1).

According to the ^1H -NMR spectrum, these crystals were composed of TMPB and acetone and the molar ratio of TMPB to acetone was 1:1.

Appearance: white crystals

Amount recovered: 30 g

Yield: 90% (based on TMPB contained in dichloromethane solution (1))

^1H -NMR (300 MHz, CDCl_3 , δ ppm): 1.20 (3H, s), 2.16 (6H, s), 3.17 (1H, ABq, $J = 16.2$ Hz), 3.66 (1H, ABq, $J = 16.2$ Hz), 4.58 (1H, ABq, $J = 14.7$ Hz), 4.59 (1H, ABq, $J = 14.7$ Hz), 4.87 (1H, s), 5.41 (1H, dd, $J = 4.2$ Hz, 1.5 Hz), 6.90 (1H, s), 7.2-7.4 (10H, m), 7.73 (2H, d, $J = 3.9$ Hz)

X-ray powder diffraction pattern (obtained with copper radiation of $\lambda=1.5418$ Å through a monochromator, same applies hereinbelow):

d (Interplanar spacings)	Relative intensities (I/I_0)
11.8405	96

	8.8556	84
	7.4935	55
	7.2487	18
	6.5438	10
5	5.9170	38
	5.5005	10
	4.8756	49
	4.7869	76
	4.6915	33
10	4.4271	100
	4.3498	75
	4.2630	26
	4.2149	27
	3.9345	42
15	3.6837	36
	3.6014	13
	3.5283	18
	3.4346	21
	3.2996	28
20	3.2734	21
	3.2065	17
	3.0640	13
	2.9878	14
	2.8951	29
25	2.8554	19

2.8448

24

Purity: 100% (determined by using liquid chromatography)

Figure 1 shows the X-ray powder diffraction pattern of the crystals obtained above.

5 Example 2

Acetone solution (1) was prepared in the same manner as in Example 1.

Acetone solution (1) was heated to 38°C, and 80 ml of *n*-hexane was added dropwise, thereby precipitating
10 crystals. This crystal-containing solution was cooled to -20°C and stirred. After sufficient crystal precipitation, the crystals precipitated were recovered by filtration and washed with 80 ml of acetone/*n*-hexane mixture (volume ratio=1:1).

15 Since the ¹H-NMR spectrum of the crystals thus obtained was identical to that of the crystals of Example 1, the crystals were verified to be of TMPB-acetone.

Appearance: white crystals

Purity: 100% (determined by using liquid chromatography)

20 Amount recovered: 32 g

Yield: 97% (based on TMPB contained in dichloromethane solution (1))

Examples 3-7

25 TMPB-acetone crystals were prepared in the same manner as in Example 2 except that various poor solvents as

shown in Table 1 below were used in place of *n*-hexane.

Since the ¹H-NMR spectra of the crystals thus obtained were identical to that of the crystals of Example 1, the crystals were verified to be of TMPB-acetone.

5

Table 1

	Poor solvent	Yield (based on TMPB contained in dichloromethane solution (1))
Ex. 3	Cyclohexane	80.5%
Ex. 4	<i>n</i> -Pentane	81.8%
Ex. 5	<i>n</i> -Octane	82.9%
Ex. 6	Diisopropyl ether	75.1%
Ex. 7	Di- <i>n</i> -butyl ether	83.8%

Example 8

10 TMPB-acetone crystals (30 g) as obtained in Example 1 were left to stand at 40°C under reduced pressure (4 kPa) for 8 hours. Based on the ¹H-NMR spectrum, the crystals thus obtained were of TMPB, with no TMPB-acetone crystals being contained in the TMPB crystals.

Appearance: white crystals

15 Amount recovered: 27 g

Yield: 90% (based on TMPB contained in dichloromethane solution (1))

X-ray powder diffraction pattern:

	d (Interplanar spacings)	Relative intensities (I/I ₀)
20	9.5016	81
	7.5574	73

	6.3658	20
	5.5623	11
	5.0578	100
	4.8545	54
5	4.7412	56
	4.6866	43
	4.5577	19
	4.4140	34
	4.3330	44
10	4.2308	47
	3.9974	25
	3.7857	10
	3.6777	20
	3.6014	29
15	3.1907	11
	3.0995	11
	2.8483	11

Purity: 100% (determined by using liquid chromatography)

Figure 2 shows the X-ray powder diffraction
20 pattern of the crystals.

Example 9

TMPB-acetone crystals (32 g) as obtained in
Example 2 were treated in the same manner as in Example 8.
Based on the ^1H -NMR spectrum, the crystals thus obtained
25 were of TMPB, and the ^1H -NMR spectrum and the x-ray powder

diffraction pattern thereof were identical to those of the crystals prepared in Example 8.

Appearance: white crystals

Amount recovered: 29 g

5 Yield: 97% (based on TMPB contained in dichloromethane solution (1))

Purity: 100% (determined by using liquid chromatography)

Example 10

TMPB-acetone crystals (32 g) as obtained in
10 Example 1 were dissolved in 240 ml of dichloromethane, and 68 ml of acetic acid was added thereto. To this mixture was added little by little 20.4 g of potassium permanganate without the temperature of the mixture exceeding 20°C, and the mixture was stirred for 3 hours while making sure that
15 the temperature of the mixture did not exceed 40°C. After completion of the reaction, 300 ml of dichloromethane was added. The mixture thus obtained was cooled to 5°C, and 35% hydrogen peroxide aqueous solution was added until the color of the mixture disappeared. The dichloromethane
20 layer was separated, washed with 2% aqueous sodium hydrogensulfite solution and then with water, and dried over magnesium sulfate. The dichloromethane layer was concentrated, and methanol was added to the residue to effect crystallization, thereby giving the desired TAZB.
25 Amount recovered: 29.7 g

Yield: 96%

Purity: 100% (determined by using liquid chromatography)

Comparative Example 1

The procedure of Example 1 was repeated to
5 obtain dichloromethane solution (1).

Dichloromethane solution (1) was concentrated
under reduced pressure (60 to 40 kPa) at 40°C. When the
amount of removed dichloromethane reached about 420 ml, 86
ml of ethyl acetate was added. Concentration was continued
10 until the amount of removed organic solvent reached 120 ml.
The concentrated solution was analyzed by gas
chromatography, and diluted with dichloromethane and ethyl
acetate to have a dichloromethane content of 20 ml and an
ethyl acetate content of 80 ml. To this diluted solution
15 was added 48 ml of *n*-hexane while maintaining the solution
temperature at 22°C or higher, thereby precipitating TMPB
crystals.

The crystals were recovered by filtration, washed
with 80 ml of ethyl acetate/*n*-hexane mixture (volume
20 ratio=1:1), and dried under reduced pressure at about 40°C.
Appearance: pale yellow crystals

Amount recovered: 19 g

Yield: 63.3%